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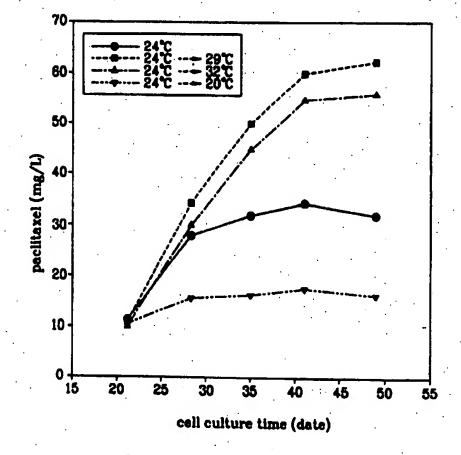
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(54) Title: MASS PRODUCTION OF PACLITAXEL BY CHANGING THE TEMPERATURE OF THE MEDIUM DURING THE PLANT CELL CULTURE

(57) Abstract

The present invention relate to a method to increase the production level of paclitaxel by changing the temperature during the plant cell culture. According to the present invention, the production of the paclitaxel comprises the following procedure: (i) cultivating the Taxus genus plant cells in a medium at ca. 20 to 25 °C; and (ii) when growth of the plant cells has progressed sufficiently, changing the cultivation temperature to ca. 26 to 32 °C to continue the culture. The present invention comprises also the method of increasing the paclitaxel production by inoculating the cells at a high initial concentration and by increasign the saccharide concentration in the medium. According to the present invention, paclitaxel can be mass-produced conveniently and therefore has an industrial application.



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WO 99/00513 PCT/KR98/00179

MASS PRODUCTION OF PACLITAXEL BY CHANGING THE TEMPERATURE OF THE MEDIUM DURING THE PLANT CELL CULTURE

BACKGROUND OF THE INVENTION

Field of the Invention

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The present invention relates to a method for mass production of paclitaxel, a secondary metabolite by plant cell culture.

Description of the Prior Art

Paclitaxel is one of taxane compounds which are isolated from the bark of *Taxus brevifolia*, and it is effective for the treatment of cancer, such as leukemia. It is reported that paclitaxel is capable of curing approximately 30 %, 50 % and 20 % of ovarian, breast and lung cancers, respectively, by inhibiting depolymerization of microtubules. Generally, paclitaxel can be produced by a total chemical synthesis, by a semi-synthesis employing precursors such as baccatin, direct extraction of paclitaxel from *Taxus* genus plants or by culturing cells that produce paclitaxel. Among these methods, plant cell culture-based process for paclitaxel production has the following advantages. First, paclitaxel can be

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produced in a continuous manner regardless of a fluctuation in the supply of yew plants due to damages by blight, and harmful insects or by natural disasters. Secondly, cell cultures can be propagated in large bioreactors, from which paclitaxel can be massively produced by manipulating culture conditions. Thirdly, cell cultures produce a simpler spectrum of compounds compared to other methods, considerably simplifying separation and purification. Fourthly, a cell culture process can adapt quickly to rapid changes in demand better than the other methods. And fifthly, a cell culture process can produce paclitaxel as well as taxane precursors such as baccatin that can be converted to paclitaxel.

Methods for producing paclitaxel by utilizing plant cell culture have been described in the art:

USP 5,019,504 discloses a method for producing paclitaxel and its derivatives utilizing cultured cells of *Taxus brevifolia*. The yield of paclitaxel described therein, however, is 1~3 mg/L with the doubling time for the biomass is 7 ~12 days which is insufficient for industrial application. Moreover, the production of paclitaxel by the plant culture is unstable and even when a primary cell having high production level is obtained by selection, it is difficult to keep its content by subculturing (E. R. M. Wickremesine et. al., World Congress on Cell and Tissue Culture (1992)).

WO 93/17121 offers a method for paclitaxel production by cell culture of *Taxus* genus plant while changing composition of the medium, growth rate, and production rate, etc. In case of *Taxus chinensis*, 24.1

mg/L of paclitaxel can be obtained in 18 days of culture and biomass doubles every 2.5 days.

All of these patents describe methods for mass production of paclitaxel by controlling the cell cultivation temperature to 25 °C; there are no teaching in said patents, nor do they anticipate that the changes in the growth rate or production rate when the cell cultivation temperature is varied.

SUMMARY OF THE INVENTION

The object of the present invention is to provide a convenient and efficient method for mass production of paclitaxel.

Another object of the present invention is to provide a convenient method for the production of paclitaxel with high yield by regulating the temperature during the plant cell culture.

Another object of the present invention is to provide a more productive method of producing paclitaxel by inoculating a strain that produces paclitaxel at a high concentration.

BRIEF DESCRIPTION OF THE DRAWINGS

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The above and other objects and features of the present invention will become apparent from the following descriptions given in conjunction with the accompanying drawings, in which:

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Figure 1 is a graph showing the effect of temperature in the growth rate of a paclitaxel producing cell line, *Taxus chinensis* SYG-1.

Figure 2 is a graph showing the effect of the temperature change during the culture of *Taxus chinensis* SYG-1 on paclitaxel production.

Figure 3 is a graph showing the effect of the time-point of the temperature change on the growth of *Taxus chinensis* SYG-1.

DETAILED DESCRIPTION OF THE INVENTION

The present invention relates to a method to increase the production level of paclitaxel by changing the temperature during the plant cell culture. More particularly, the present invention comprises a mass production method for obtaining paclitaxel with a high yield by changing the temperature of the culture media for incubation after the growth of the *Taxus* genus plant cells are sufficiently progressed.

In general, the production of a secondary metabolite from a plant is not related to its growth. Some of the secondary metabolites participate in the protection of the plant from environmental stress. In case of the plant cell culture, one can improve the production of the secondary metabolite by regulating the metabolism that is related to the defense mechanism of the plant. In the present invention, a method to maximize the production level

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of paclitaxel by changing the temperature during the plant cell culture is developed. Also in the present invention, a method of increasing the production of paclitaxel is developed by increasing the initial number of cells for inoculation and by adjusting the concentration of saccharide in the cell culture medium based on the knowledge that the initial number of cells for the inoculation and the initial concentration of saccharide can affect the metabolism.

The inventors first optimized the temperature for the cell growth, and then tried to find the cultivation temperature in order to increase the production level of paclitaxel by retarding the cells growth. To this end, the inventors have cultivated the *Taxus* genus plant cells at the optimum growth temperature until sufficient cells were obtained and subsequently grew the cells at a changed temperature to increase the production level of the secondary metabolites including paclitaxel.

According to the present invention, the production of the paclitaxel comprises of the steps of:

- (i) cultivating the *Taxus* genus plant cells in a medium at about 20 to 25 °C, preferably at about 20 to 24 °C; and,
- (ii) when the growth of the plant cells has progressed sufficiently, changing the cultivation temperature to about 26 to 32 °C, preferably to about 28 to 30 °C and continuing the cultivation to produce paclitaxel.

The time-point for the sufficient cell growth can vary depending on the kind of plant cell, the cultivation temperature, the composition of the

medium or other conditions. According to the Examples of the present invention, the cell cultivation temperature can be changed 10 days, preferably 14 days or more preferably 21 days after the initiation of the culture.

According to the methods of the present invention, paclitaxel production is increased when cultivation temperature is increased after the cell growth were progressed sufficiently at a slightly low temperature. After inoculating the cells, it is desirable to change the temperature to 26 to 32 °C which is higher than the growth temperature, preferably to 28 to 30 °C. It is considered that the changed temperature could be optimum for the production or the activity of the enzymes that participate in the biosynthesis of paclitaxel.

The methods in the present invention is applied to any plants of Taxus genus without any particular limitations. For instance, the method of the present invention can be applied to Taxus brevifolia, Taxus canadensis, Taxus cuspidata, Taxus baccata, Taxus globosa, Taxus floridana, Taxus wallichiana, Taxus x media and Taxus chinensis.

The medium for the plant cell culture in the present invention is B5 medium supplemented with casein hydrolysate (Gamborg et. al., Exp. Cell Res. 50: 151-158 (1968)). To increase the paclitaxel production level, it is preferable to use the modified B5 medium as shown in Table 1. Moreover, a saccharide, preferably maltose can be added to the medium at day 5 to day 30, at least once and preferably twice; once at day 7 to 12 and another

at day 18 to day 24 after the initiation of the culture at a concentration of 10 to 100 g/L, preferably of 10 to 40 g/L for a single dose.

Table 1

Taxus genus plant cell culture medium

composition	concentration (mg/L)
inorganic salts	
CaCl₂ anhydride	113.23
CoCl ₂ .6H2O	0.025
CuSO₄.5H₂O	0.025
FeSO₄.7H₂O	27.8
H ₃ BO ₃	3.0
KI	0.75
KNO ₃	2,500
MgSO ₄ .7H ₂ O	246
MnSO ₄ .H ₂ O	10
NaH ₂ PO ₄ .H ₂ O	150
Na ₂ MoO ₄ .2H ₂ O	0.25
(NH ₄) ₂ SO ₄	134
ZnSO₄.7H₂O	2
vitamins	
inositol	10
nicotinic acid	1
calcium pentosenate	0.874

	pyridoxin.HCl	1
	riboflavin	0.015
	thyamine.HCl	10
	hormones	
5 .	naphthalene acetate	10 μΜ
	benzylaminopurin	0.2 μΜ
	casein hydrolysis product	500
	AgNO ₃	1-15 μΜ
	sucrose	30,000
	· •	

Another method in the present invention comprises the step of inocultating the cells at a higher concentration than normal, for instance at 4 g/L of the dried cell mass. In case the inoculating cells at a higher concentration, it is desirable that the saccharide concentration in medium to be higher than in normal culture, for instance, 40 g/L.

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The present invention is further illustrated in the following examples, which should not be taken to limit the scope of the invention.

Example 1: Effect of the cultivation temperature on the growth of the *Taxus* genus cells and paclitaxel production.

Taxus chinensis Hu-1, Taxus chinensis SYG-1 (KCTC-0232BP),
Taxus baccata, Taxus x media and Taxus cuspidata cultures were
cultivated for 15 days in B5 medium supplemented with 500 mg/L of casein

hydrolysate. Each cell culture was inoculated to 75 ml of the medium in Table 1 in a 250 ml Erlenmeyer flask and cultivated for 20 days at 24 °C. At day 21, the cultivation temperature was changed to 29 °C. The dried cell mass and the amount of produced paclitaxel at days 21 and 42 were measured, and the results are showed in Table 3.

The dried cell mass was measured by the following method.

First, a 5.5 cm filter paper (No. 541, Whatman Co. U.S.A.) was put on a porous funnel equipped with a suction flask. The filter paper was attached on the funnel fully by squirting distilled water thereto. Then, 5 ml of the plant cell culture medium to be analyzed was spread on the filter paper and filtered under reduced pressure to remove the water. The filter paper after the suction was put on a dish made with aluminum foil and dried in an oven at 80°C for 24 hours. After this procedure, the filter paper was taken out of the oven and left at room temperatures for 10 min before measuring the total weight of the aluminum foil-dish and the filter paper. By subtracting this value from the pre-determined weight of the aluminum foil-dish and the filter paper and subsequently by multiplying 200 to the result to obtain the dried cell mass per one liter of the culture medium.

The amount of paclitaxel produced was quantitatively analyzed by HPLC using the conditions in Table 2.

Table 2

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Conditions for quantitative analysis of paclitaxel

Instrument	HPLC(Waters, U.S.A.)
Column	Capcell Pack C18 UG120 (length: 250 mm, inner
	diameter: 4.6 mm)
Column temperature	40 °C
Mobile phase	acetonitrile:water (20 % - 100 % gradient)
Fluid speed	1.0 ml/min
Injection volume	10 µl
Detector	UV (227 nm), ATTE = 3)

Table 3

Effect of the temperature changes on the growth of the *Taxus* genus plant cells and the production level of paclitaxel.

		Dried cell mass (g/L)		Paclitaxel (mg/L)	
		Day 21	Day 42	Day 21	Day 42
T. baccata	Culture at 24 °C	7.8	10.1	0.3	0.6
	24 °C->29 °C	7.3	10.4	0.3	0.7
T. chinensis Hu-1	Culture at 24 °C	7.5	11.1	0.9	1.7
	24 °C->29 °C	7.3	9.5	0.8	2.9
T. chinensis SYG-1	Culture at 24 °C	14.3	18.1	25.1	46.7
	24 °C->29 °C	14.1	18.5	24.3	93.2
T. cuspidata	Culture at 24 °C	8.5	12.4	0.5	1.1
	24 °C->29 °C	8.1	11.9	0.8	2.3

T. x media	Culture at 24 °C	11.6	14.2	3.4	7.6
	24 °C->29 °C	10.9	14.7	3.2	13.2

Example 2: Temperature effect on the plant cell growth

SYG-1 cell culture which had been cultivated previously for 15 days in B5 medium supplemented with 500 mg/L of casein hydrolysate was inoculated to 75 ml of the medium in Table 1 hydrolysate in a 250 ml Erlenmeyer flask, and cultivated for 20 days at 20 °C, 24 °C, 29 °C, 32 °C and 36 °C. The dried cell mass was measured by using the method in Example 1 to determine the optimum growth temperature. The results of the dried cell mass is shown in Figure 1 (-•-:20 °C; -=-:24 °C; -_-:29 °C; -_-:36 °C).

As can be seen in Figure 1, the dried cell mass for the plant cells grown at 20 °C, 24 °C, 29 °C, 32 °C and 36 °C were 8.23, 12.3, 6, 4.5 and 3.8 g/L, respectively, at day 13.

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Example 3: Effect of the temperature change during the plant cell culture on the cell growth and the production level of paclitaxel.

To determine the temperature change at which the cells were continuously grown after the cells were grown sufficiently at 24 °C, the plant cell, *Taxus chenensis* SYC-1 was grown continuously under the following conditions: (1) temperature of the medium was 24 °C during the culture

(hereinafter, referred to as '24 °C control group' for convenience); (2) temperature of the medium was 24 °C up to day 21 and changed to 29 °C (24 °C - 29 °C test group); (3) temperature of the medium was 24 °C up to day 21 and changed to 32 °C (24 °C - 32 °C test group); (4) temperature of the medium was 24 °C up to day 21 and changed to 20 °C (24 °C - 20 °C test group). The dried cell mass and the amount of produced paclitaxel were analyzed.

SYG-1 cell culture which had been cultivated previously for 14 days in B5 medium supplemented with 500 mg/L of casein hydrolysate was inoculated to 75 ml of the medium in Table 1 hydrolysate in a 250 ml Erlenmeyer flask, and cultivated at 24 °C. After 7 days, 10 g/L of maltose was added to each flask to continue the culture. At day 21, 20 g/L of maltose were added to all of the flasks. At day 21, among the 4 test groups, the cultivation temperature was maintained at 24 °C for one of the group. For the other groups, the temperature was changed to 29 °C (24 °C - 29 °C test group); to 32 °C (24 °C - 32 °C test group) and to 20 °C (24 °C - 20 °C test group) respectively, and cultivated continuously. After finishing the cell culture, 7 ml of the culture from each group was sampled to determine the dried cell mass and the amount of paclitaxel produced according to the method described in Example 1. The results are shown in Table 4 and Figure 2. (-•- 24 °C control group; -•- :24 °C - 29 °C test

group; -_-:24 °C - 32 °C test group; -_-: 24 °C - 20 °C test group). The 24 °C - 29 °C test group had the highest paclitaxel production level.

Table 4

Effect of the temperature change on growth

Temperature change at	Dried cell mass (g/L)			
day 21	day 21	day 42		
24 °C	14.1	18.1		
from 24 °C to 29 °C	14.2	19.2		
from 24 °C to 32 °C	14.2	17.9		
from 24 °C to 20 °C	14.5	15.8		

Example 4: Effect of the time-point of the temperature change on the growth and the paclitaxel production

The cells were cultivated as described in Example 3 except that the time-point of the temperature change and the cultivation temperature were varied. The dried cell mass and the amount of paclitaxel produced were analyzed.

The dried cell mass and the amount of produced paclitaxel were determined for the groups that were cultivated at 24 °C for 49 days, at 29 °C for 49 days, at 29 °C from day 8, at 29 °C from day 15 and at 29 °C from day 22 by using the method described in Example 1. The results are shown in Figure 3 and In Table 5.

Table 5

Effect of the time-point of the temperature change on the amount of the produced paclitaxel.

Time-point of temperature change	Produced Paclitaxel (mg/L)		
	21st day	49th day	
24 °C for 49 days	26.0	28.8	
29 °C for 49 days	17.8	76.5	
24 °C for 7 days, 29 °C from 8th day	32.2	74.9	
24 °C for 14 days, 29 °C from 15th day	45.8	110.3	
24 °C for 21 days, 29 °C from 22nd day	26.7	137.5	

Example 5. Effect of inoculation at a high concentration

Effect of inoculation at a high concentration and the temperature change during the culture on the growth and the paclitaxel production level were determined. In Test group 1, the SYG-1 cells were cultivated in B5 medium supplemented with 500 mg/L of casein hydrolysate for 14 days, inoculated in the medium in Table 1 at a 1:4 ratio and cultivated at 24 °C for 14 days and subsequently cultivated at 24 °C after adding 3 % maltose. In Test group 2, all of the conditions were identical as in Test group 1 except that the cultivation temperature was changed to 29 °C after the 14th day. In the Test group 3, the cells were concentrated twice for the inoculation and cultivated at 24 °C. In the Test group 4, all of the conditions were identical

as in Test group 3 except that the cultivation temperature was changed to 29 °C after the 14th day. The dried cell mass and the amount of produced paclitaxel were determined for the 4 Test groups at day 14, at day 28 and at day 42. The results are shown in Tables 6 and 7.

Table 6

Dried cell mass of Test groups inoculated at high concentration (g/L).

Test group	. 1	2	3	4
Day				
day 14	9.36	9.00	11.19	11.23
day 28	15.12	14.68	15.94	17.49
day 42	17.03	18.34	15.03	16.42

Table 7

Content of paclitaxel (mg/L) and production level per unit dried cell mass

(mg/g) of Test groups inoculated at high concentration.

Test group	1	2	3	4
Day				
day 14	1.54 mg/L	1.30 mg/L	8.7 mg/L	8.0 mg/L
	0.16 mg/g	0.14 mg/g	0.78 mg/g	3.01 mg/g
day 28	23.05 mg/L	30.65 mg/L	39.87 mg/L	47.57 mg/L
	1.52 mg/g	2.09 mg/g	2.50 mg/g	2.72 mg/g
day 42	32.90 mg/L	48.35 mg/L	35.87 mg/L	51.83 mg/L
· · · · ·	1.93 mg/g	2.65 mg/g	2.39 mg/g	3.16 mg/g

Example 6. Effect of high concentration inoculation and high saccharide concentration.

The effects of inoculating the cells at a high concentration along with the effect of the temperature change during the culture and of a high saccharide concentration were observed. In Test group 1, the SYG-1 cells were cultivated in B5 medium supplemented with 500 mg/L of casein hydrolysate for 14 days, inoculated in the medium in Table 1 at a 1:4 ratio and cultivated at 24 °C for 14 days and subsequently cultivated at 24 °C after adding 3 % maltose. In Test group 2, the medium contained 6 % maltose initially, and the maltose was not replenished during the culture. In Test group 3, all the conditions were identical as in Test group 1 except that the cells were concentrated twice for the inoculation. In the Test group 4, all of the conditions were identical as in Test group 3 except that the cultivation temperature was changed to 29 °C after the 14th day. The dried cell mass and the amount of produced paclitaxel were determined for the 4 Test groups at day 14, day 28 and day 42. The results are shown in Tables 8 and 9.

Table 8

Dried cell mass when inoculated at high concentration (g/L).

	- •			
Test group	1	2	3 .	4
Day				
day 14	9.36	6.34	9.63	9.65

day 28	15.12	15.88	12.75	14.22
day 42	17.03	11.24	12.37	15.74

Table 9

Content of paclitaxel (mg/L) and production level per unit dried cell mass (mg/g) of the Test groups inoculated at a high concentration.

Test group	. 1	2	3	4
day				
day 14	1.54 mg/L	1.95 mg/L	13.57 mg/L	16.40 mg/L
	0.16 mg/g	0.31 mg/g	1.41mg/g	1.70 mg/g
day 28	23.05 mg/L	48.80 mg/L	48.13 mg/L	79.40 mg/L
	1.52 mg/g	3.07 mg/g	3.77 mg/g	5.58 mg/g
day 42	32.90 mg/L	42.20 mg/L	33.20 mg/L	78.23 mg/L
	1.93 mg/g	3.75 mg/g	2.68 mg/g	4.97 mg/g

As clearly illustrated and demonstrated as above the present invention provides an efficient method for mass production with a high yield of paclitaxel that can be applied industrially.

What is claimed is:

1. A method for mass production of paclitaxel by changing a cultivation temperature that comprises the steps of:

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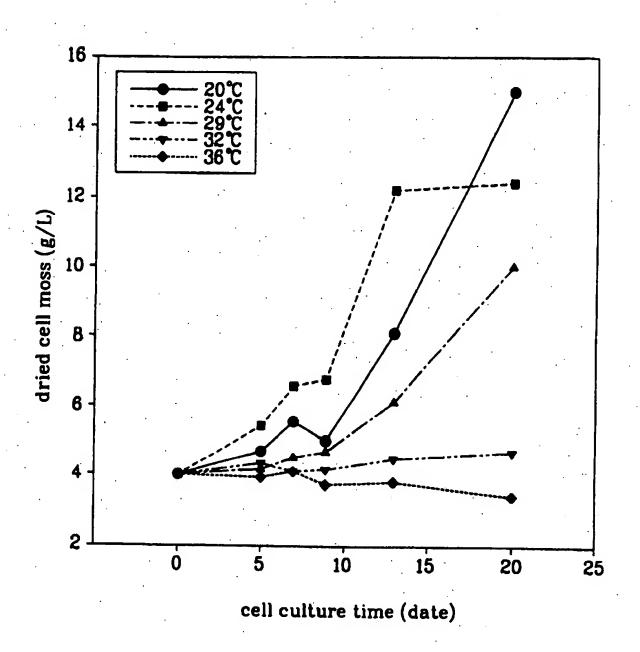
- (i) cultivating Taxus genus plant cells at 20 to 25 °C; and
- (ii) when a growth of the plant cells has progressed sufficiently after the initiation of the cultivation, changing the cultivation temperature to 26 to 32 °C to continue the cultivation.

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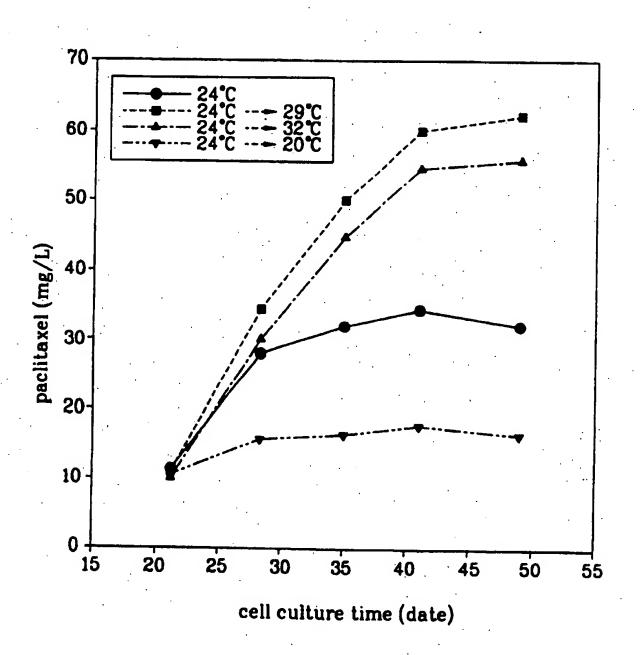
- 2. The method for mass production of paclitaxel according to Claim 1, wherein the cultivation temperature is changed at or later than day 10 after the initiation of the culture.
- 3. The method for mass production of paclitaxel according to Claim 1, wherein 10 to 100 g/L of carbon source is supplied to the culture at days 5 through 30 after the initiation of the culture at least once is additionally included.
- 4. The method for mass production of paclitaxel according to Claim 1, wherein the concentration of *Taxus* genus plant cells is greater than or equal to 4 g/L as a dried weight for the inoculation in step (i).

5. The method for mass production of paclitaxel according to Claim 4, wherein said culture in step(I) is conducted in a medium containing saccharide at a concentration higher than 40 g/L.

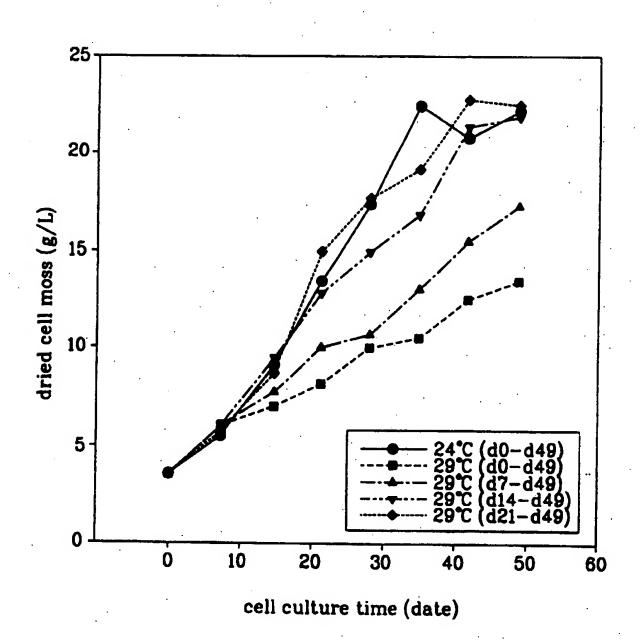
1/3 FIG. 1



2/3 FIG.2



3/3 FIG.3



INTERNATIONAL SEARCH REPORT

International application No.
PCT/KR 98/00179

A. CLASSIFICATION OF SUBJECT MATTER IPC : C 12 P 17/02 According to International Patent Classification (IPC) or to both national classification and IPC B. FIELDS SEARCHED Minimum documentation searched (classification system followed by classification symbols) IPC : C 12 P 17/02 Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched Electronic data base consulted during the international search (name of data base and, where practicable, search terms used) WPI, EPODOC C. DOCUMENTS CONSIDERED TO BE RELEVANT Category Citation of document, with indication, where appropriate, of the relevant passages Relevant to clain A. WO 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A. US 5 019 504 A (CHRISTEN et al.) 28 May 1991 (28.05.91), claims 1,2.	n No.
According to International Patent Classification (IPC) or to both-national classification and IPC B. FIELDS SEARCHED Minimum documentation searched (classification system followed by classification symbols) IPC C 12 P 17/02 Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched Electronic data base consulted during the international search (name of data base and, where practicable, search terms used) WPI, EPODOC C. DOCUMENTS CONSIDERED TO BE RELEVANT Category* Citation of document, with indication, where appropriate, of the relevant passages Relevant to clai A W0 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A US 5 019 504 A (CHRISTEN et al.) 28 May 1991 1 (28.05.91), claims 1,2.	n No.
Minimum documentation searched (classification system followed by classification symbols) IPC 6: C 12 P 17/02 Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched Electronic data base consulted during the international search (name of data base and, where practicable, search terms used) WPI, EPODOC C. DOCUMENTS CONSIDERED TO BE RELEVANT Category* Citation of document, with indication, where appropriate, of the relevant passages Relevant to claim A WO 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A US 5 019 504 A (CHRISTEN et al.) 28 May 1991 (28.05.91), claims 1,2.	n No.
Minimum documentation searched (classification system followed by classification symbols) IPC 6: C 12 P 17/02 Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched Electronic data base consulted during the international search (name of data base and, where practicable, search terms used) WPI, EPODOC C. DOCUMENTS CONSIDERED TO BE RELEVANT Category Citation of document, with indication, where appropriate, of the relevant passages Relevant to claim A WO 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A US 5 019 504 A (CHRISTEN et al.) 28 May 1991 (28.05.91), claims 1,2.	n No.
Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched Electronic data base consulted during the international search (name of data base and, where practicable, search terms used) WPI, EPODOC C. DOCUMENTS CONSIDERED TO BE RELEVANT Category* Citation of document, with indication, where appropriate, of the relevant passages Relevant to claim A WO 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A US 5 019 504 A (CHRISTEN et al.) 28 May 1991 1 (28.05.91), claims 1,2.	n No.
Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched Electronic data base consulted during the international search (name of data base and, where practicable, search terms used) WPI, EPODOC C. DOCUMENTS CONSIDERED TO BE RELEVANT Category* Citation of document, with indication, where appropriate, of the relevant passages Relevant to claim A WO 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A US 5 019 504 A (CHRISTEN et al.) 28 May 1991 1 (28.05.91), claims 1,2.	n No.
Electronic data base consulted during the international search (name of data base and, where practicable, search terms used) WPI, EPODOC C. DOCUMENTS CONSIDERED TO BE RELEVANT Category Citation of document, with indication, where appropriate, of the relevant passages Relevant to clair A WO 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A US 5 019 504 A (CHRISTEN et al.) 28 May 1991 1 (28.05.91), claims 1,2.	n No.
Electronic data base consulted during the international search (name of data base and, where practicable, search terms used) WPI, EPODOC C. DOCUMENTS CONSIDERED TO BE RELEVANT Category* Citation of document, with indication, where appropriate, of the relevant passages Relevant to clair A WO 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A US 5 019 504 A (CHRISTEN et al.) 28 May 1991 1 (28.05.91), claims 1,2.	n No.
C. DOCUMENTS CONSIDERED TO BE RELEVANT Category* Citation of document, with indication, where appropriate, of the relevant passages Relevant to claim A WO 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A US 5 019 504 A (CHRISTEN et al.) 28 May 1991 (28.05.91), claims 1,2.	n No.
C. DOCUMENTS CONSIDERED TO BE RELEVANT Category* Citation of document, with indication, where appropriate, of the relevant passages Relevant to claim A WO 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A US 5 019 504 A (CHRISTEN et al.) 28 May 1991 (28.05.91), claims 1,2.	n No.
C. DOCUMENTS CONSIDERED TO BE RELEVANT Category* Citation of document, with indication, where appropriate, of the relevant passages Relevant to claim A WO 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A US 5 019 504 A (CHRISTEN et al.) 28 May 1991 (28.05.91), claims 1,2.	n No.
Category* Citation of document, with indication, where appropriate, of the relevant passages Relevant to claim A WO 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A US 5 019 504 A (CHRISTEN et al.) 28 May 1991 (28.05.91), claims 1,2.	n No.
Category* Citation of document, with indication, where appropriate, of the relevant passages Relevant to claim A WO 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A US 5 019 504 A (CHRISTEN et al.) 28 May 1991 (28.05.91), claims 1,2.	n No.
A WO 97/21 696 A1 (XECHEM, INC.) 19 June 1997 (19.06.97), abstract. A US 5 019 504 A (CHRISTEN et al.) 28 May 1991 (28.05.91), claims 1,2.	n No.
(19.06.97), abstract. US 5 019 504 A (CHRISTEN et al.) 28 May 1991 (28.05.91), claims 1,2.	
(28.05.91), claims 1,2.	
A WO 93/17 121 A1 (PHYTON CATALYTIC, INC.) 02 September 1993 (02.09.93), claims 1-5.	
	•
Further documents are listed in the continuation of Box C. See patent family annex.	
Special categories of cited documents:	
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International application No.

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angeführ Pater in : Documer	echerchenbericht rtes Patentdokument ntes Patentdokument document cited search report nt de brevet cité rapport de recherche	Datum der Veröffentlichung Publication date Date de publication	Mitglied(er) der Patentfamilie Patent family member(s) Membre(s) de la famille de brevets	Datum der Veröffentlichung Publication date Date de publication
WO A:	1 9721696	19-06-97	AU A1 74848/96 BR A 9607137 CA AA 2210972 CN A 1182424 EP A1 809639 US A 5654448	03-07-97 25-11-97 19-06-97 20-05-98 03-12-97 05-08-97
US A	5019504	28-05-91	keine – nohe – r	ien
WO A1	9317121	02-09-93	AU A1 37291/93 AU B2 672194 EP A1 672162 EP A4 672162 JP T2 7506721 NZ A 249734 SG A1 46427 US A 5407816	13-09-93 26-09-96 20-09-95 29-11-95 27-07-95 27-08-96 20-02-98 18-04-95